



AUBURN UNIVERSITY

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COLLEGE OF ENGINEERING

AEROSPACE

AERO 4970/7970

Rocket Propulsion I
Heat Transfer Analysis of Rocket Systems

SET III

1. Compute the total or stagnation temperature that would occur ideally at the nose of a vehicle flying at an altitude of 25 km and a Mach number of 6. Assume isentropic conditions, an ambient air temperature of 203K, $k=1.4$, and a molecular mass of 29 kg/kmol.

Answer: 1,665 K.

2. How much total heat per second can be absorbed in a thrust chamber with an inside wall surface area of 0.2 m^2 if the coolant is aniline and the coolant does not exceed $145 \text{ }^\circ\text{C}$ in the jacket? Assume the average specific heat of aniline to equal 0.45 kcal/kg-K , an inlet temperature of $26 \text{ }^\circ\text{C}$, and a coolant flow of 2 kg/s . What is the average heat transfer rate per second per unit area?

3. During a static test, a certain thrust chamber is cooled by water. The following data are given:

Average water temperature	$100 \text{ }^\circ\text{F}$
Thermal conductivity of water	$1.07 \times 10^{-4} \text{ Btu/sec-ft-}^\circ\text{F}$
Gas temperature	$4500 \text{ }^\circ\text{F}$
Viscosity of water	$2.5 \times 10^{-5} \text{ lb-sec/ft}^2$
Specific heat of water	$1 \text{ Btu/lb-}^\circ\text{F}$
Cooling passage dimensions	$\frac{1}{4} \times \frac{1}{2} \text{ in}$
Water flow through passage	0.585 lb/sec
Thickness of inner wall	$\frac{1}{8} \text{ in}$
Heat absorbed	$1.3 \text{ Btu/in}^2\text{-sec}$
Thermal conductivity of wall material	$26 \text{ Btu/hr-ft-}^\circ\text{F}$

Determine: (a) the film coefficient of the coolant; (b) the wall temperature on the coolant side; and (c) the wall temperature on the gas side.

4. In Problem 3, determine the water flow required to decrease the wall temperature on the gas side by $100 \text{ }^\circ\text{F}$. What is the percentage increase in coolant velocity? Assume that the various properties of the water and the average water temperature do not change.

5. Determine the absolute and relative reductions in wall temperatures and heat transfer caused by applying insulation in a liquid-cooled rocket chamber with the following data:

Tube wall thickness	0.381 mm
Gas temperature	2760 K
Gas-side wall temperature	1260 K
Heat transfer rate	15 MW/m ²
Liquid film coefficient	23 kW/m ²
Wall material (see table below)	Stainless steel AISI type 302

An 0.2 mm thick layer of insulating paint is applied on the gas side; the paint consists mostly of magnesia particles. The conductivity of this magnesia is 2.59 W/m-K.

	Copper, Com. Pure		Aluminum Alloy, 24S-T		Low Carbon Steel, SAE 1020		Alloy Steel, SAE X4130		Stainless Steel, AISI Type 302		Nickel Alloy, Inconel	
Ultimate tensile strength (psi)	75°F	33,000	75°F	68,000	85°F	62,400	75°F	98,300	75°F	93,000	75°F	85,000
			212	62,000	900	45,500	600	87,000	200	83,000	200	81,000
			500	26,000	1000	36,500	800	84,000	600	76,200	600	79,000
			600	15,000	1200	20,000	1000	65,000	1000	65,600	1000	79,000
			700	7500	1300	13,500			1400	31,800	1400	47,000
				1400	9025				1600	15,700	1600	23,000
									2000	4700	1800	15,000
									2300	2300	2000	11,000
Yield strength (psi)	Annealed		Short time test				Normalized		Annealed		Short time test	
	75°F	10,000	75°F	45,000	85°F	42,000	75°F	74,000	75°F	37,000	75°F	36,000
			400	35,000	900	23,500	400	73,600	200	29,700	200	32,000
			500	23,000	1000	20,100	800	66,000	600	22,000	600	27,000
			600	13,000	1300	7375	900	59,300	1000	17,100	1000	22,000
			700	6500	1400	3750	1000	53,400	1400	14,900	1400	19,000
Modulus of elasticity (psi × 10 ⁶)	Annealed		0.02% offset				Normalized		Annealed		0.2% offset	
	75°F	16.0	75°F	10.3	70°F	29.5	70°F	29.5	85°F	27.5	75°F	31.0
			212	10.0	400	24.5	400	24.5	900	23.4	500	28.7
			300	9.78	600	21.5	600	21.5	1000	22.2	1000	25.0
			400	9.27	800	18.5	800	18.5	1200	20.7	1350	21.0
			500	8.24	1000	15.5	1000	15.5	1400	18.3	1500	18.5
				1200	12.5	1200	12.5	1500	13.3			
Thermal conductivity (Btu/hr ft ² °F/in.)	32°F	2648.6	64°F	1567.0	32°F	360.5	32°F	298.1	32°F	110	86°F	124.8
	392	2579.3			392	339.7	392	291.2	392	119	392	131.7
	752	2516.9			752	298.1	752	270.4	752	136	1472	194.1
	1112	2392.1			1472	179.6	1112	235.7	1112	159	2192	249.6
					1832	187.2	1472	180.3	1472	180		
				2012	194.1	1832	194.1	1832	194			
				2192	208.0	2192	208.0	2192	206			
Coefficient of thermal expansion (in./in. °F × 10 ⁻⁶)	32°F	8.83	68-212°F	12.9	68- 212°F	6.5	32- 212°F	7.04	32- 212°F	8.23	50°F	5.6
	572	10.91	68-392	13.3	68- 392	6.7	32- 572	7.48	32- 572	9.50	200	6.8
	752	11.86	68-572	13.7	68- 572	7.1	32- 932	7.88	32- 932	10.02	400	8.0
	932	12.94			68- 932	7.7	32-1292	8.24	32-1292	10.43	600	8.7
	1112	14.15			68-1112	8.0	32-1652	7.23	32-1652	10.67	800	9.3
1472	16.97			68-1292	8.2	32-1832	7.70	32-1832	10.75	1000	10.1	
							32-2012	8.04		1400	10.2	
Specific heat (Btu/°F lb)	75°F	0.0918	64-212°F	0.212	68°F	0.115	212°F	0.114	212°F	0.122	78-212°F	0.109
	392	0.096			572	0.133	572	0.130	572	0.131		
	752	0.100			932	0.150	932	0.157	932	0.142		
	1472	0.109			1292	0.152	1292	0.197	1292	0.149		
	1832	0.114			1652	0.154	1472	0.211	1652	0.156		
				2012	0.156	1832	0.145	2012	0.158			
				2372	0.166	2282	0.154	2282	0.162			
Melting point	1981.4°F	Approx. 2700°F	Approx. 2780°F	Approx. 2700°F	2550°F	2540°F						